



Hydrogen Pathways Course

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Hydrogen Production
Lecture 2

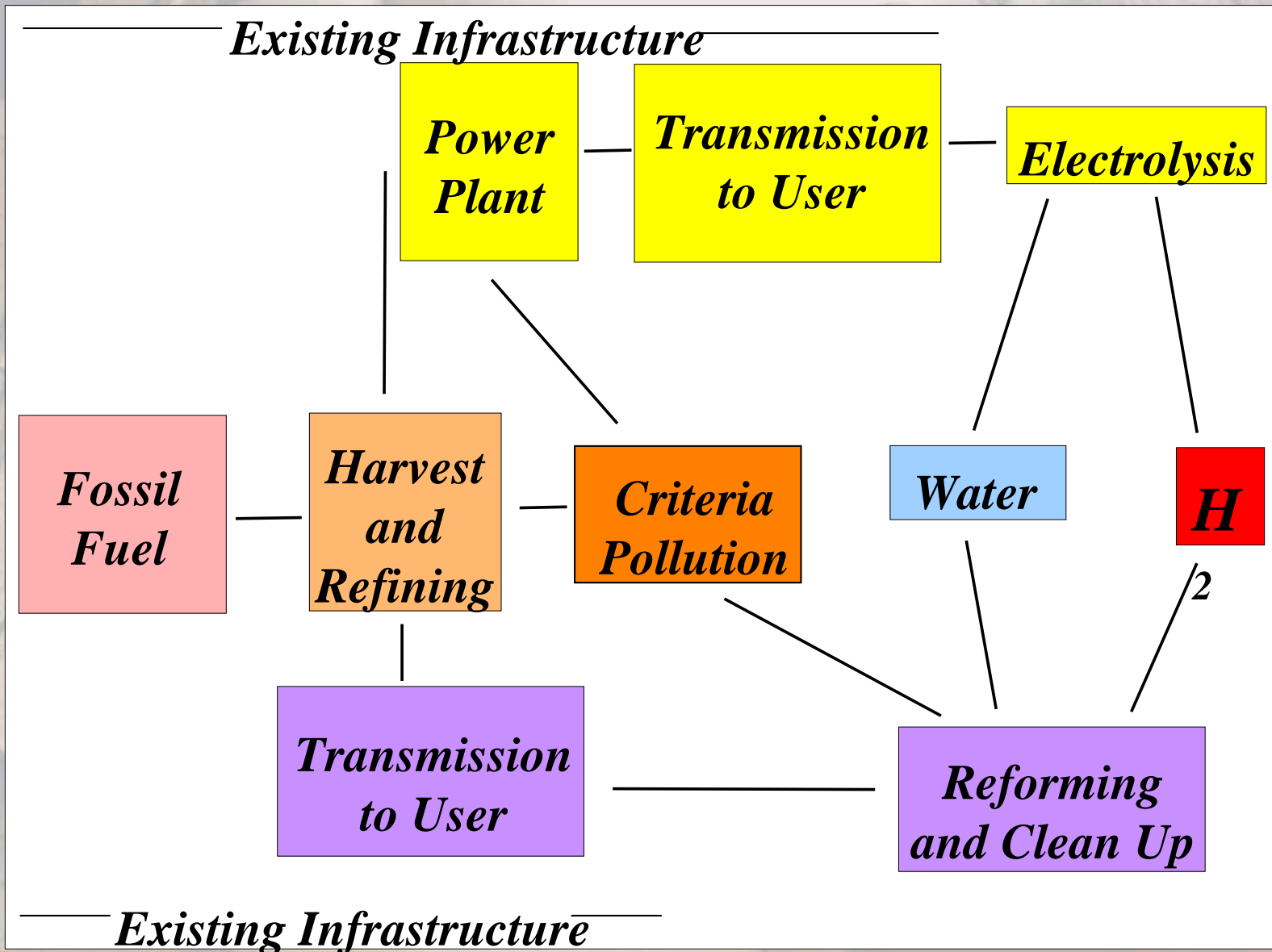
Today's Lecture

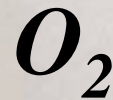
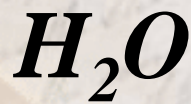
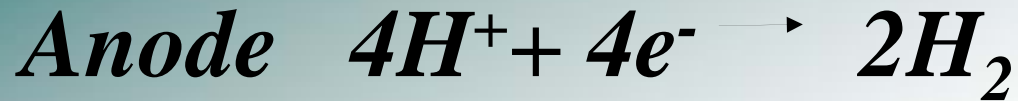
Hydrogen Production

\$ Direct Methods of Solar to Hydrogen Production via Water-splitting

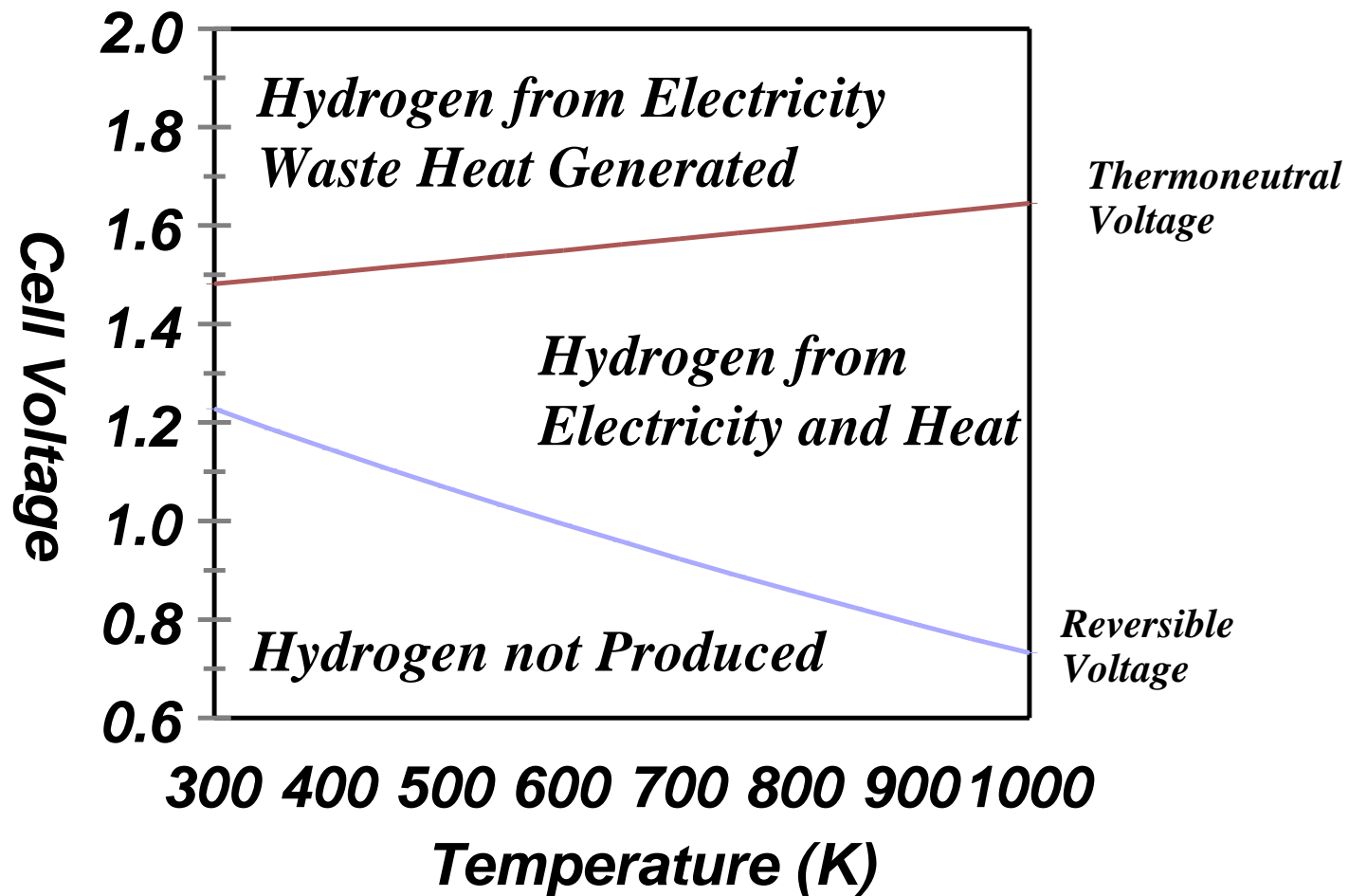
- ② Photoelectrical***
- ② Photochemical***
- ② Thermochemical***
- ② Thermal decomposition***

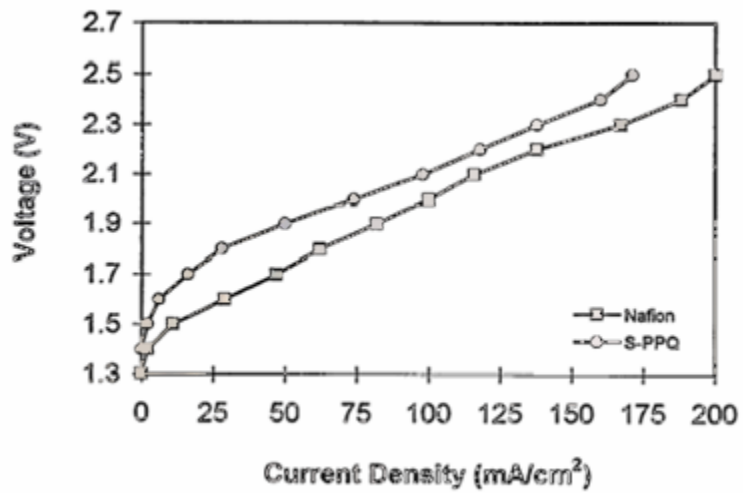
Current Production of Hydrogen



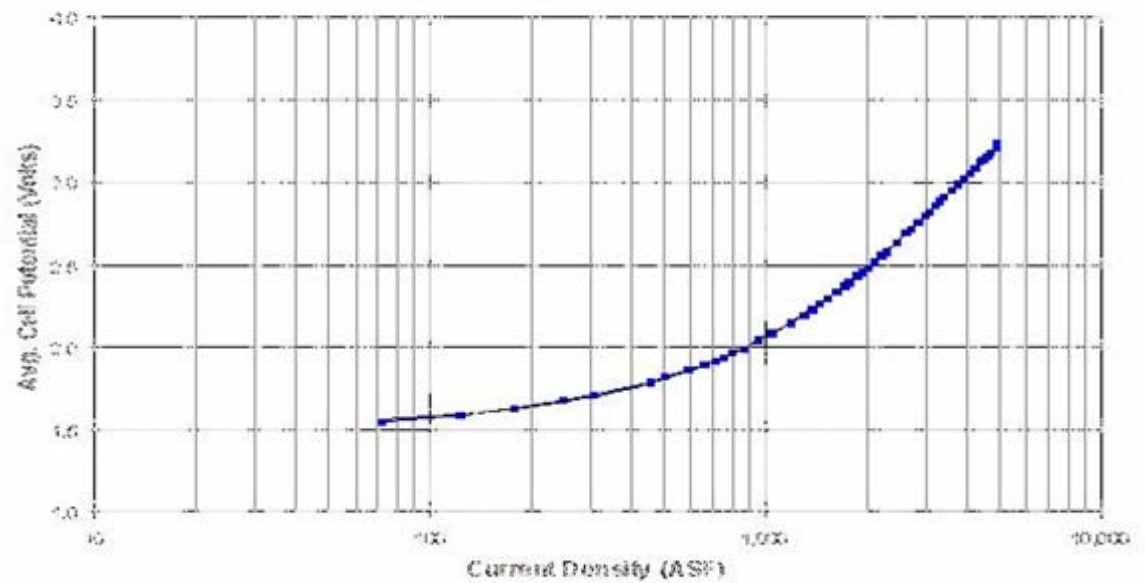


Electricity

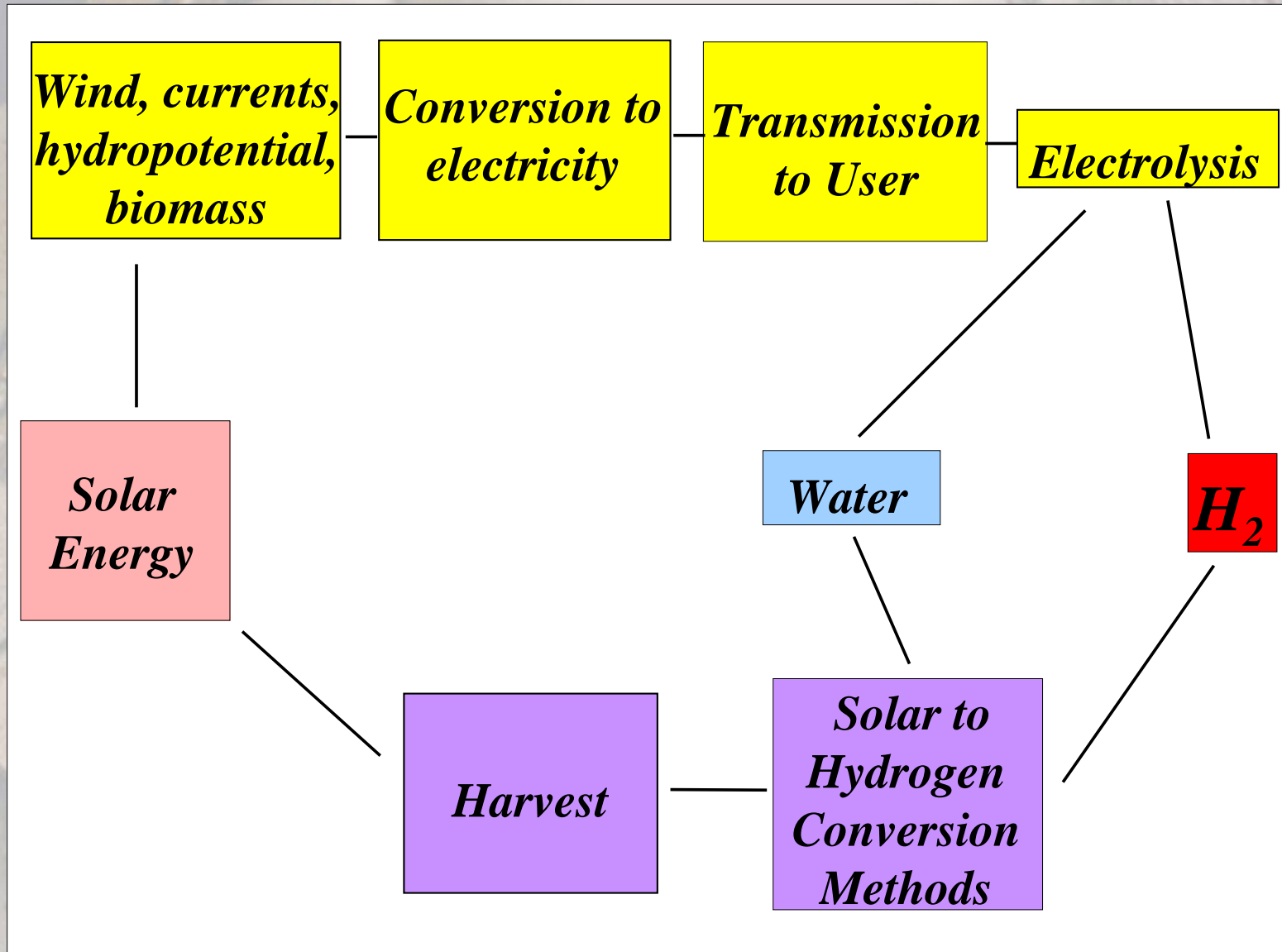




Cell Stack Polarization
 6.00 m², 2-cell stack, 200 psig, NRC/MO200202



Renewable Hydrogen Production



Methods of Hydrogen Production with Solar Energy Conversion

\$Photoconversion

- ② *Photovoltaics with Electrolysis*
- ② *Photoelectrochemical*
- ② *Biological*

\$Thermal Conversion

- ② *Solar Heat Engines with Electrolysis*
- ② *Thermal Decomposition*
- ② *Thermochemical Cycles*

\$Hybrid cycles



Schatz Energy Center



Sandia National Lab

Photovoltaics with Electrolysis

Sunlight-Photovoltaics-Electrolysis-H₂

\$Conceptually elegant (low voltage DC)

\$Demonstrated and commercial

\$Low conversion efficiency due to photovoltaic conversion

@Multijunction PV can boost efficiency

\$Cost

*Schatz Hydrogen
Generating Station*



Solar Heat Engines with Electrolysis

*Sunlight-Concentrator-Heat Engine-Generator-
Electrolysis-H₂*

*\$ Can use well known cycles such as
Rankine, Brayton, or Stirling*

\$ High conversion efficiency

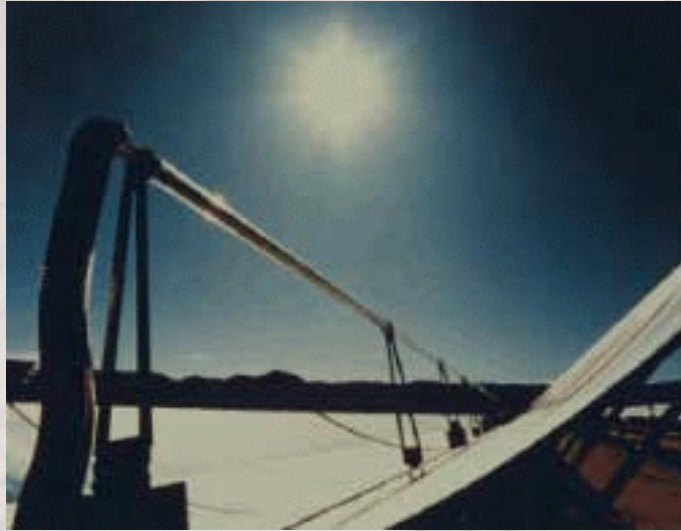
*\$ Requires high concentration ratios for
high temperatures (Carnot limited thermal
cycles)*

*\$ Additional conversion step (kinetic to
electrical)*

*\$ Intermittent nature of sunlight can
complicate heat engine (numerous start-
ups and shutdowns)*

Solar Heat Power Systems for Hydrogen Production

*Parabolic
Concentrator
SEGS
Power plants*



Dish Stirling



*Heliostats
Power Tower
Solar 1*

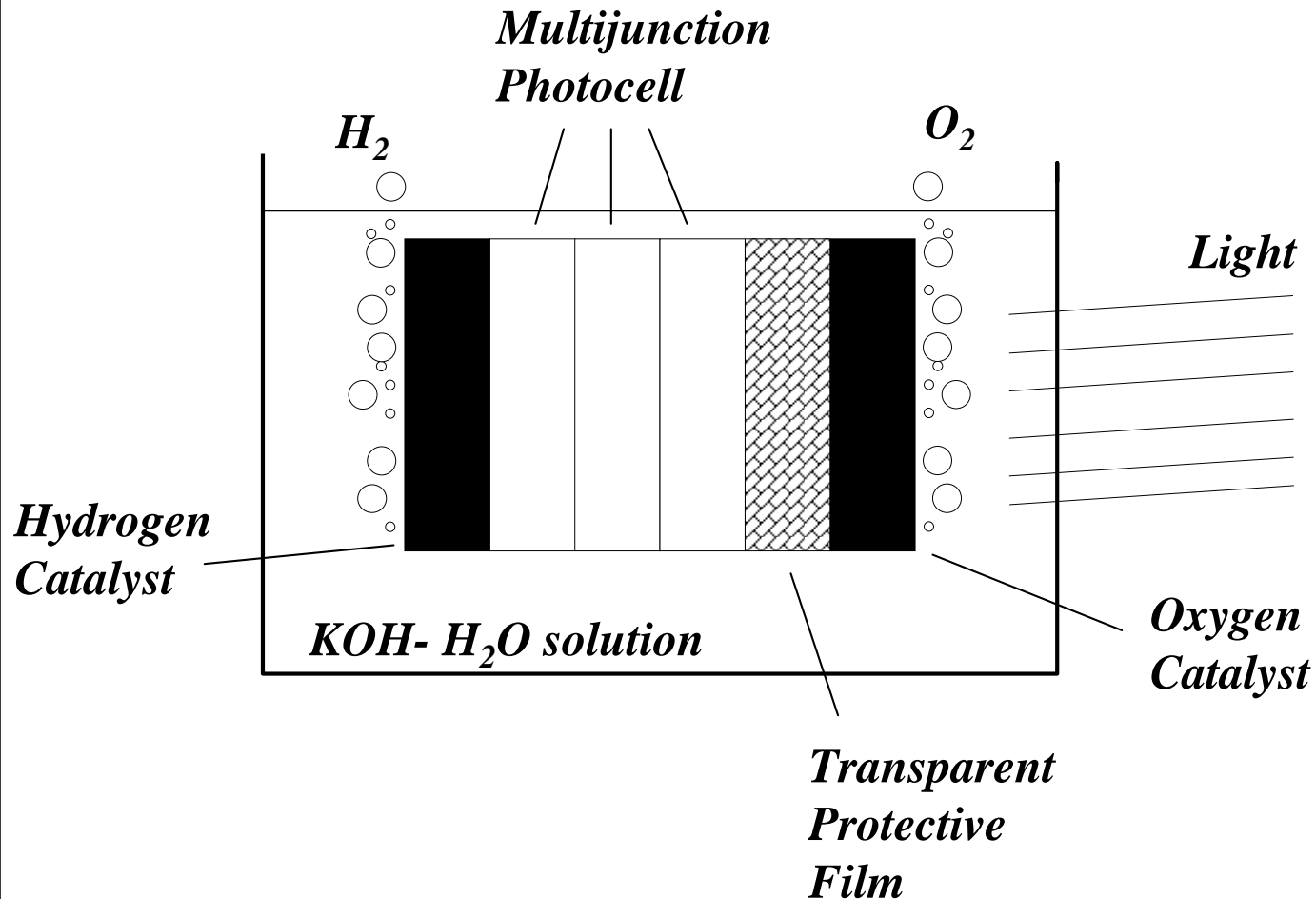


*Hydrogen generating system
by Proton Energy Systems*

Photoelectrochemical

Sunlight-Photoelectrochemical Cell-H₂

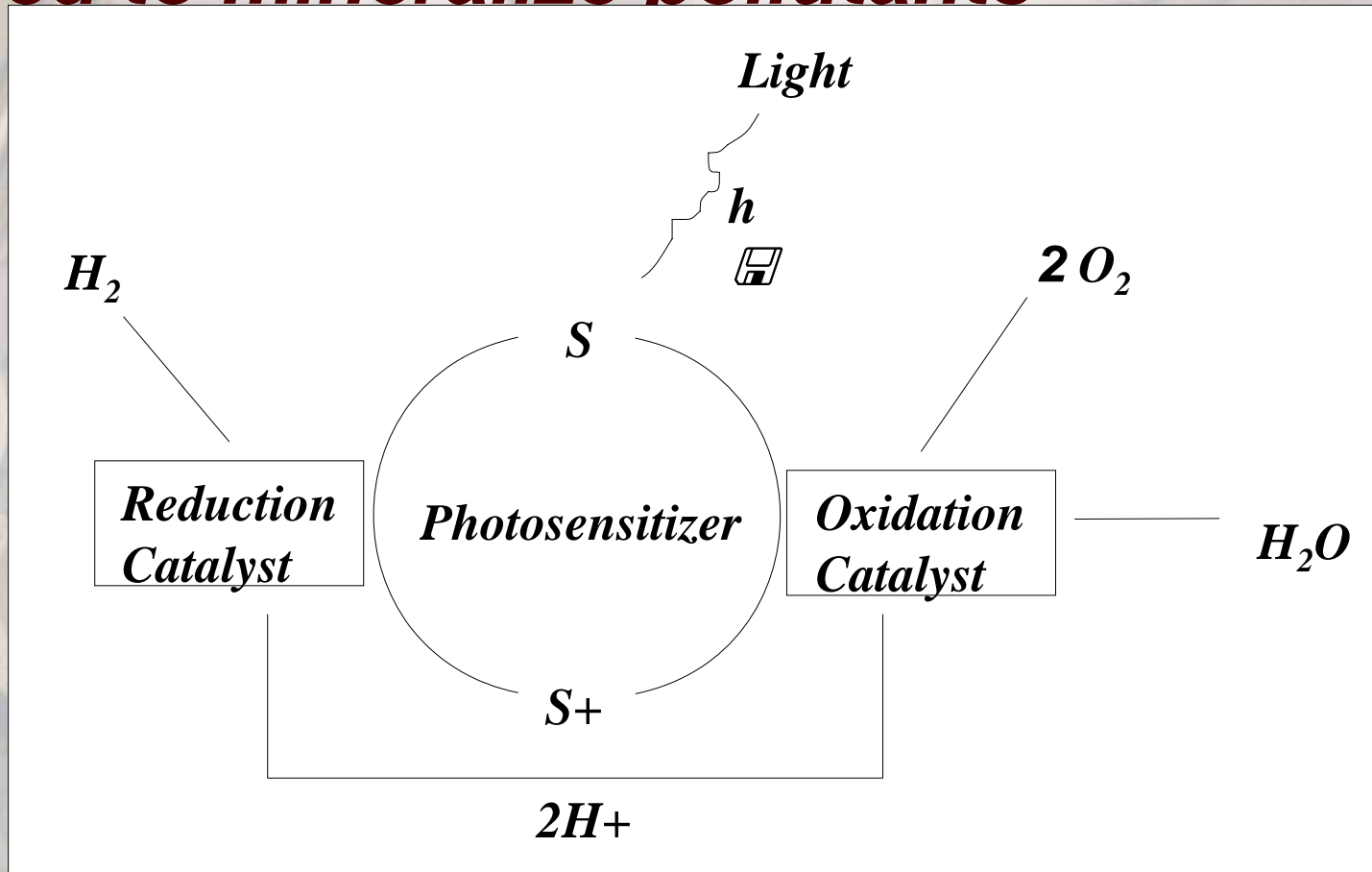
\$ Miniaturization and marriage of PV-



Photochemical

Sunlight-Chemical Solution- H_2/O_2 -Separator- H_2

Photochemical systems can also be used to mineralize pollutants



Thermal Decomposition

Sunlight-Concentrator-High Temperature Reactor-

Separator-H₂

\$Separation of High Temperature Mixture

\$Reactor Materials

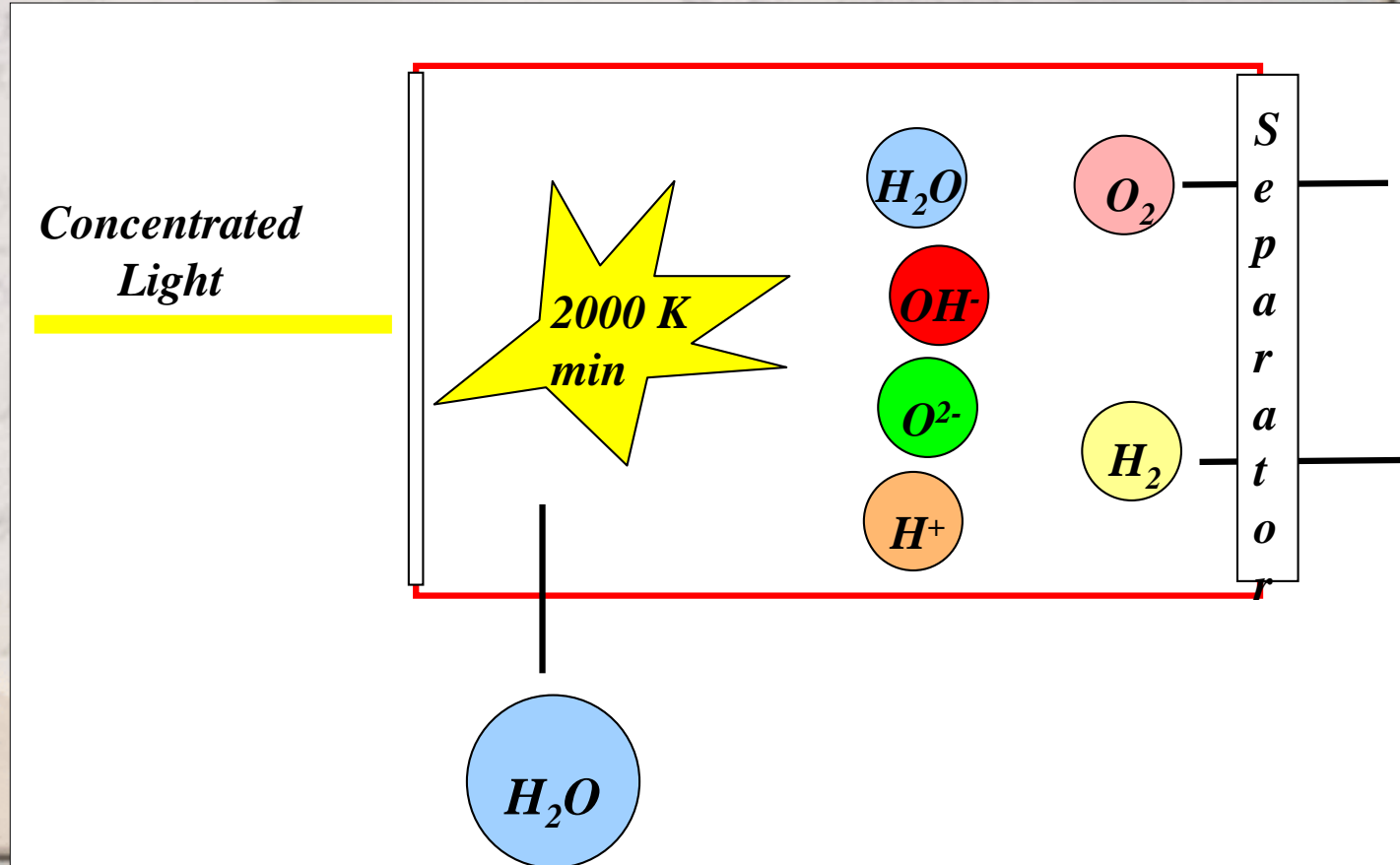


Table 2 Equilibrium Mole Fractions of a Water Mixture at Different Pressures and Temperatures

Temperature	2000 K		
Pressure	1 atm	0.1 atm	0.02 atm
H	0.0001	0.0006	0.0016
H ₂	0.0058	0.0124	0.0209
H ₂ O	0.9896	0.9773	0.9607
O	0.0000	0.0002	0.0004
OH	0.0021	0.0042	0.0075
O ₂	0.0024	0.0052	0.0088
Temperature	2500 K		
Pressure	1 atm	0.1 atm	0.02 atm
H	0.0052	0.0230	0.0627
H ₂	0.0428	0.0843	0.1259
H ₂ O	0.9110	0.8059	0.6685
O	0.0018	0.0081	0.0226
OH	0.0233	0.0464	0.0705
O ₂	0.0160	0.0322	0.0497
Temperature	3000 K		
Pressure	1 atm	0.1 atm	0.02 atm
H	0.0578	0.2114	0.4153
H ₂	0.1352	0.1811	0.1398
H ₂ O	0.6440	0.3239	0.1021
O	0.0244	0.0914	0.1866
OH	0.0914	0.1260	0.1010
O ₂	0.0470	0.0062	0.0552

General Thermochemical Cyclic Process

$AB + H_2O \xrightarrow{\text{Heat}} AH_2 + BO$ Water Consumption

$2BO \xrightarrow{\text{Heat}} O_2 + 2B$ Oxygen Production

$AH_2 \xrightarrow{\text{Heat}} A + H_2$ Hydrogen Production

$A + B \xrightarrow{\text{Heat}} AB$ Material Regeneration

3000+ cycles

Materials

Build-up or depletion of intermediate compounds

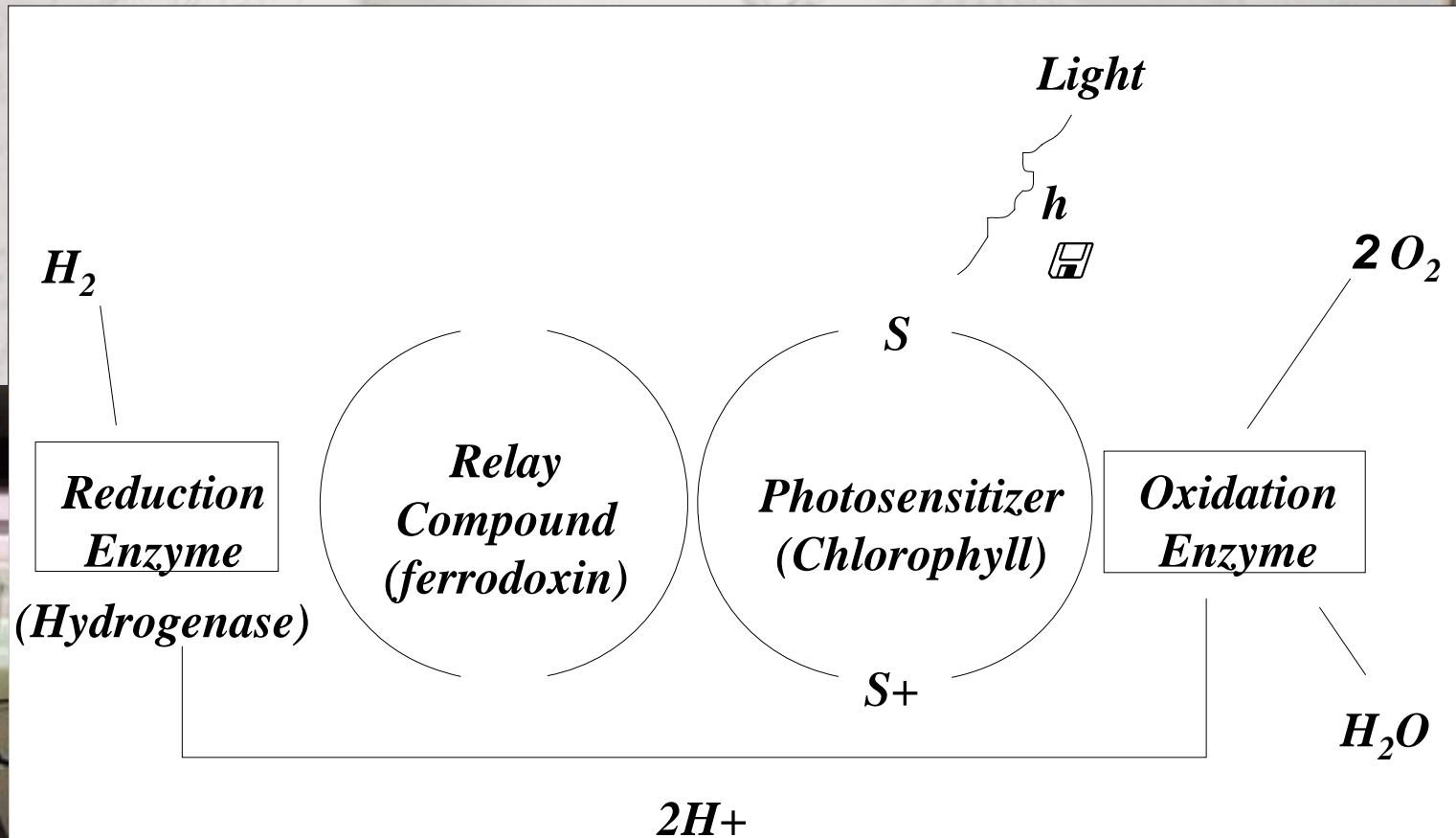
Toxicity of intermediate compounds

Biological Methods

Sunlight-Bioreactor-Separator-H₂

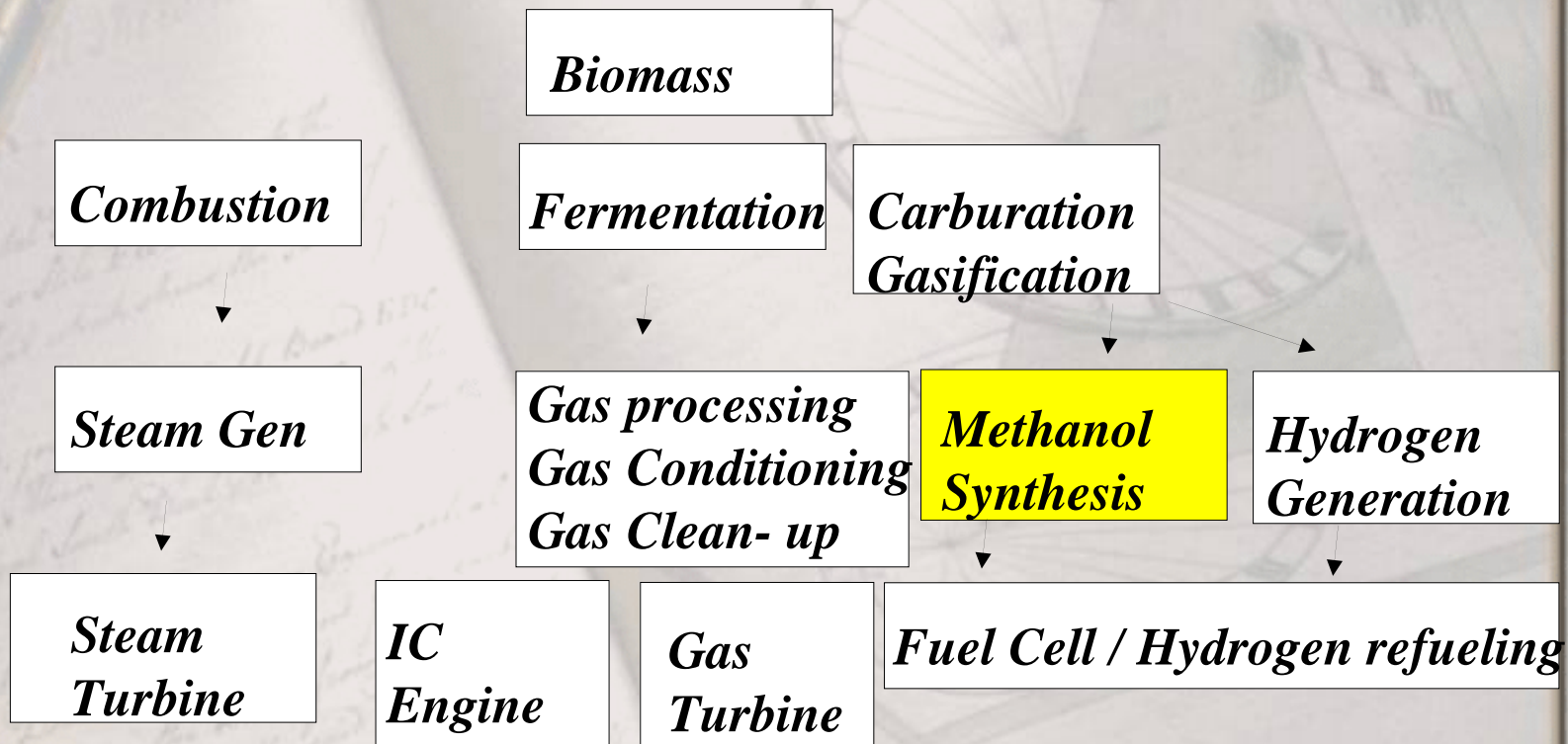
\$Saturation at about 0.3 suns

\$Oxygen sensitivity



Energy Production Via Biomass

Sources



Biogas Pathway

*Biogas 60% Methane
37% CO₂
1-2% Hydrogen*

Removal of Sulphur

Absorbtion on Fe-O or Zn-O

Absorbtion on Activated Carbon

Removal of Halogens

Absorbtion on Activated Carbon

Removal of Siloxanes

*Cooling to -2C
Absorbtion on Activated Carbon*

Removal of Moisture

Drier

SOFC or MCFC

Removal of Solids

*60% Methane
37% Carbon Dioxide*

*Convert Biogas to
CO and H₂*

*Steam-Reforming
Partial Ox
Autothermal Reforming*

PAFC

CO Conversion

Water-gas Shift

PEMFC

Low Level CO removal

*PSA
PROX
Membrane Purification*

Efficiencies and Estimated Costs

Method	Theoretical Efficiency	Achieved Efficiency	Estimated Cost	DOE goal
PV electrolysis	27.8%	13% Calculated for Multi-junction PV	41\$/GJ	9-14 \$/GJ
Solar heat engine and electrolysis	36%	18.8% Calculated for Dish Stirling	46 \$/GJ projected Power Tower	
Photoelectro- chemical	31% Single Photosystem	12.4% Concentrated light	24 \$/GJ projected	
Thermal Decomposition	40%	2.1%	??	
Biological	31%	11% Transient only	??	
Thermochemical cycles	~40%	18% From Heat only	??	
Fossil Based Hydrogen Production	N/A	N/A	10\$/GJ	6-8 \$/GJ